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黑钨矿有效沉淀机制: CO₂ 逃逸

刘向冲^{1,2},张德会³

(1. 中国地质科学院地质力学研究所,北京 100081;

2. 中国地质科学院地质力学研究所动力成岩成矿实验室,北京 100081;

3. 中国地质大学(北京)地球科学与资源学院,北京 100083)

摘 要:黑钨矿是石英脉钨矿床的主要矿石矿物,其沉淀机制一直存在争议。CO₂逃逸能否造成 黑钨矿有效沉淀尚缺乏定量模型的评价。文章建立了 W-Fe-Cl-Na-O-C-H 体系的反应平衡模型, 涉及 22 种组分和 16 个化学反应;相关热力学参数来自 SUPCRT 数据库。模型计算结果表明, pH 与流体压力呈负相关关系,而钨溶解度与流体压力呈正相关关系;当成矿流体压力从静岩压 力降至静水压力水平,钨溶解度降幅可达到 27%~47%,降幅与温度和深度成正比。因而,降压 造成的 CO₂逃逸是黑钨矿沉淀的有效机制之一。

关键词:黑钨矿;沉淀机制;CO2逃逸;平衡反应模型

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THE EFFICIENT MECHANISMS FOR PRECIPITATING WOLFRAMITE: CO, ESCAPING

LIU Xiangchong^{1,2}, ZHANG Dehui³

(1. Institute of Geomechanics, Chinese Academy of Geological Sciences, Beijing 100081, China;

2. The Laboratory of Dynamic Digenesis and Metallogenesis, Institute of Geomechanics, CAGS, Beijing 100081, China;

3. School of Earth Sciences and Resources, China University of Geosciences (Beijing), Beijing 100083, China)

Abstract: Wolframite is the main ore mineral of vein-type tungsten deposits. How wolframite precipitates from hydrothermal fluids is highly disputed in the literature. Whether CO_2 escaping causes significant precipitation wolframitehas not been quantitatively examined. A reaction equilibrium model for the system of W-Fe-Na-Cl-H-C-O was established in this contribution. The model contains 22 species and 16 reactions, the thermodynamic data of which are from the database SUPCRT. The modeling results indicate that pH is negatively correlated to fluid pressure and tungsten solubility is positively correlated to fluid pressure from lithostatic to hydrostatic level could cause a drop of tungsten solubility by $27\% \sim 47\%$, and the decrease degree has a positive correlation to temperature and depth. Therefore, CO_2 escaping accompanying a drop of fluid pressure is one of the mechanisms precipitating wolframite efficiently.

Key words: wolframite; precipitation mechanism; CO, escaping; equilibrium reaction modeling

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钨矿是一种岩浆热液型矿床,主要的矿石矿 物有白钨矿和黑钨矿^[1-2]。其中,黑钨矿主要赋存 在石英脉型黑钨矿床,其沉淀机制存在争议^[3~5]。 柳志青^[3]根据黑钨矿在石英脉中的分布规律,提 出矿物微粒浓差运离分带的假说, 定性地解释黑 钨矿集合体 (钨砂包) 的牛长机制。有学者提出 钨成矿流体为富硅的岩浆热液过渡性流体,而非 简单的热水溶液^[4,6~7]。一些学者利用流体包裹体、 稳定同位素、高温高压实验和计算模拟等方法提 出黑钨矿可能有四种沉淀方式:①简单降温[8~9]; ②岩浆水与大气降水混合^[10];③水岩反应^[11]; ④流体不混溶^[12-14]。其中,流体不混溶的证据主 要来自含 CO₂ 的流体包裹体,这种包裹体在南岭 地区锡田^[15]、盘古山^[16]、大吉山^[17]、茅坪^[18]等 多个石英脉型钨矿中发现。Liu^[19]利用计算模拟发 现,水力破裂后热液中 CO。的溶解度可下降 36%。 然而,降压后 CO,逃逸如何改变热液化学平衡和 钨溶解度有待定量模型的进一步评价。文章通过 NaCl-H,O-CO,体系反应平衡模型定量分析 CO,逃 逸对钨溶解度的影响,以探讨其是否为黑钨矿有 效沉淀机制。

1 研究背景

石英脉型黑钨矿床是重要的钨矿床类型之一, 主要分布于江西、湖南、广东、广西等地^[2,4,6]。 含黑钨矿的石英脉近垂直分布在碱长花岗岩顶部 接触带附近^[20],延伸约1km^[21-23]。矿石矿物和脉 石矿物的流体包裹体研究结果表明钨成矿流体是 NaCl-H₂O±CO₂体系,成矿温度一般在 300 °C ~ 400 °C,压力可达 90~200 MPa,盐度通常不超过 10wt% NaCl,相关实验数据来自大吉山^[8,17]、瑶岗 仙^[9,24,25]、锡田^[11]、盘古山^[16,26]、茅坪^[18]、海锡 坑^[27,28]、漂塘^[29,30]、黄沙^[31]、西华山^[32,33]等石英 脉型 钨矿床。该类型矿床的产出深度约 4~ 8 km^[5,32,34]。

目前已在黑钨矿、黄玉、石英等矿石和脉石 矿物中发现含 CO₂ 的包裹体,相关研究表明 CO₂ 逃逸触发的流体不混溶是黑钨矿沉淀的重要机 制^[18,35-36]。CO₂ 是热液中一种较为常见的挥发 份^[37-39],也是热液酸碱平衡的缓冲剂^[40]。压力降 低会使热液中 CO₂ 逃逸,引起 pH 升高,从而可能 造成矿物质沉淀^[13,40]。故有必要定量地评价 CO, 逃逸对黑钨矿溶解度的影响。

2 反应平衡模型

地球化学反应平衡模型是以平衡热力学和反 应动力学为理论基础,利用数值计算方法,求解 相应的非线性方程组,得出研究体系中化学组分 的存在形式、浓度和活性等有关信息^[41]。该方法 已在斑岩型铜矿^[42~44]、不整合型铀矿^[45-46]、热液 型金矿[47]等多种类型矿床的成矿作用动力学机制 研究中发挥重要作用。有学者曾利用含钨体系的 反应平衡模型定量分析在钨溶解度与温度、压力、 盐度和 pH 的关系,其中 Heinrich^[48]研究了锡钨在 盐水体系的溶解度模型, Gibert 等^[49] 和龚庆杰 等^[50]的平衡反应模型主要针对白钨矿,而 Wood 和 Sammon^[51]关于黑钨矿和白钨矿的溶解度模型最 为全面;然而,以往的模型都未考虑 CO,在水溶 液的离解反应。文章通过建立 W-Fe-Cl-Na-O-C-H 体系的反应平衡模型,定量分析 CO2 逃逸对钨溶 解度的影响。

反应平衡模型考虑了 H^{\dagger} 、 OH^{-} 、 HCl^{0} 、 Cl^{-} 、 Na^{+} , $NaCl^{0}$, $NaOH^{0}$, $H_2WO_4^{0}$, HWO_4^{-} , WO_4^{2-} , $NaWO_4^-$, $NaHWO_4^0$, Fe^{2+} , $FeCl^+$, $FeCl_2^0$, $FeOH^+$, FeO^{0} , $HFeO_{2}$, $FeWO_{4}$ (s), CO_{2} (aq), HCO_{3} 7 CO3⁻ 共 22 种组分, 涉及 16 个化学反应 (表 1) 及 4个电荷和质量守恒方程(表2)。FeWO₄(s)离 解常数、NaWO₄和 NaHWO₄的缔合常数根据 Wood 和 Samson^[51]提出经验公式计算,其余 13 个化学反 应的平衡常数根据 SUPCRT 数据库的热力学参数计 算^[52]。CO,溶解度根据毛世德^[53]提出的公式计 算。有电荷组分的活度系数根据扩展 Deby-Hückel 方程计算^[54]; CO, 的活度系数根据 Drummond 提 出的经验方程计算^[55],其余电中性组分的活度系 数为1。上述平衡常数计算和非线性方程组求解在 开源程序 R 下完成。模型所用参数分别为:温度 300~400 ℃, 压力 40~200 MPa、盐度 10wt% NaCl,静水压力梯度 10 MPa/km,静岩压力梯度 25 MPa/km, 深度 4~8 km。利用 R 语言程序包 CHNOSZ 计算表 1 中的反应平衡常数和有电荷组分 的活度系数。FeWO₄(s)和CO₅(aq)不必求解, 故有 20 个变量,上述 20 个非线性方程求解利用 R 语言程序包 rootSolve 完成。

表 1 平衡反应模型中的 16 个化学反应

Fable 1	The	16	reactions	used	$_{\mathrm{in}}$	$_{\mathrm{the}}$	thermodynamic
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model of this study				
序号	化学反应			
1	$\mathrm{H}^{+} + \mathrm{WO}_{4}^{2-} = \mathrm{HWO}_{4}^{-}$			
2	$\mathbf{H}^{+} + \mathbf{H} \mathbf{W} \mathbf{O}_{4}^{-} = \mathbf{H}_{2} \mathbf{W} \mathbf{O}_{4}^{0}$			
3	$H^+ + Cl^= HCl^0$			
4	$H_2 O = H^+ + OH^-$			
5	$FeWO_4$ (s) = $Fe^{2+} + WO_4^{2-}$			
6	$\mathrm{Fe}^{2+} + \mathrm{Cl}^{=} \mathrm{Fe}\mathrm{Cl}^{+}$			
7	$\mathrm{Fe}^{2+}+2\mathrm{Cl}^{=}\mathrm{FeCl}_{2}^{0}$			
8	$\mathrm{Fe}^{2+} + \mathrm{H}_{2}\mathrm{O} = \mathrm{FeOH}^{+} + \mathrm{H}^{+}$			
9	$Fe^{2+} + H_2O = FeO^0 + 2H^+$			
10	$Fe^{2+} + 2H_2O = HFeO_2^- + 3H^+$			
11	$Na^+ + Cl^- = NaCl^0$			
12	$Na^+ + H_2O = NaOH^0 + H^+$			
13	$Na^+ + WO_4^{2-} = NaWO_4^-$			
14	$Na^+ + HWO_4^- = NaHWO_4^0$			
15	CO_2 (aq) $+H_2O = HCO_3^- + H^+$			
16	$HCO_{3}^{-} = CO_{3}^{2-} + H^{+}$			

3 计算结果

平衡反应模型计算结果如下:

(1) 在热液温度达到 300 ℃时, CO₂ 溶解度 可达到 2~10 mol/kg H₂O (图 1a); CO₂ 溶解度与 压力成正相关关系; 当流体压力从静岩压力降至 静水压力水平, CO₂ 溶解度下降 55%~57%。相比 300 ℃的溶解度线, 400 ℃热液的 CO₂ 溶解度显著 提高,最高可达到 25 mol/kg H₂O (图 1b); 当流 体压力从静岩压力降至静水压力水平, CO₂ 溶解度 下降 74%~82%。

(2) pH 与压力呈负相关关系(图 2)。300 ℃ 的热液 pH 为 3.08~3.91;当流体压力从静岩压力 降至静水压力水平,热液 pH 上升 0.4~0.5。400 ℃ 的热液 pH 范围是 3.58~5.42;当流体压力从静岩

表 2 平衡反应模型中所用的电荷和质量平衡方程

Table 2	Mass and	charge	balance	constraints	used i	n the	thermodynamic	model
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序号	名称	电荷和质量平衡方程
17	电荷平衡方程	$ \left[\begin{array}{c} \mathrm{H}^{+} \end{array} \right] \ + \ \left[\begin{array}{c} \mathrm{Na}^{+} \end{array} \right] \ + \ \left[\begin{array}{c} \mathrm{FeCl}^{+} \end{array} \right] \ + 2 \ \left[\begin{array}{c} \mathrm{Fe}^{2^{+}} \end{array} \right] \ + \ \left[\begin{array}{c} \mathrm{FeOH}^{+} \end{array} \right] \ = \ \left[\begin{array}{c} \mathrm{HWO}_{4}^{-} \end{array} \right] \ + 2 \ \left[\begin{array}{c} \mathrm{WO}_{4}^{2^{-}} \end{array} \right] \ + \ \left[\begin{array}{c} \mathrm{Cl}^{-} \end{array} \right] \ + \ \left[\begin{array}{c} \mathrm{OH}^{-} \end{array} \right] \ + \ \left[\begin{array}{c} \mathrm{HFeO}_{2}^{-} \end{array} \right] \ \end{array}] $
		+ $[HCO_3^-]$ +2 $[CO_3^{2-}]$
18	氯质量平衡方程	$\Sigma Cl = [Cl^{-}] + [HCl^{0}] + [NaCl^{0}] + [FeCl^{+}] + 2 [FeCl_{2}^{0}]$
19	$\Sigma Fe = \Sigma W$	$ [H_2WO_4^0] + [HWO_4^-] + [WO_4^{2-}] = [FeCl^+] + [FeCl_2^0] + [Fe^{2+}] + [FeOH^+] + [FeO^0] + [HFeO_2^-] $
20	CO_2 含量固定	在给定的温度、压力和盐度条件下, CO ₂ 含量达到溶解度(根据文献 [53] 公式计算)



图 1 在 4~8 km 深度的静岩压力和静水压力下 CO₂ 溶解度等温变化曲线

Fig. 1 The isothermal change of CO_2 solubility under the lithostatic and hydrostatic levels at a depth of $4 \sim 8$ km

压力降至静水压力水平, 热液 pH 上升0.9~1.2。

(3) 钨溶解度与压力呈正相关关系(图3)。
当热液温度达到 300 ℃,钨溶解度 8.19×10⁻⁶~
18.05×10⁻⁶;压力从静岩压力降至静水压力水平后,钨溶解度下降3.08×10⁻⁶~7.88×10⁻⁶,降幅
27.3%~43.7%,平均降幅 36.0%。400 ℃的热液
钨溶解度 59.97×10⁻⁶~155.41×10⁻⁶;流体压力从

静岩压力降至静水压力水平后,钨溶解度下降 33.80×10⁻⁶~72.50×10⁻⁶,降幅36%~47%,平均 降幅41%。降幅比例与深度成正比。

(4) 由图 4 可知, 含钨组分以 HWO_4^{-} 为主, 其次为 $NaWO_4^{-}$ 、 $NaHWO_4^{0}$ 、 $H_2WO_4^{0}$ 和 WO_4^{2-} 。压力 从静岩压力降至静水压力水平后, HWO_4^{-} 的浓度显 著下降。



图 2 在 4~8 km 深度的静岩压力和静水压力下 pH 等温变化曲线

Fig. 2 The isothermal change of pH under the lithostatic and hydrostatic levels at a depth of 4~8 km



图 3 在 4~8 km 深度的静岩压力和静水压力下钨溶解度等温变化曲线 Fig. 3 The isothermal change of tungsten solubility under the lithostatic and hydrostatic levels at a depth of 4~8 km



图 4 在 4~8 km 深度的静岩压力和静水压力下含钨组分等温变化曲线 Fig. 4 The isothermal change of tungsten species under the lithostatic and hydrostatic levels at a depth of 4~8 km

4 讨论与结论

目前估算南岭石英脉型黑钨矿成矿流体 pH 的 研究极少,少量国外报道的 pH 约为4~6^[51]。这与 模型中 400 ℃的热液 pH 范围接近,但高于 300 ℃ 的热液 pH。已发表的数据表明大吉山钨矿和盘古 山钨矿成矿流体的 CO₂ 含量已接近饱和状态^[16-17], 因而模型计算的 pH 可作为实际值的下限值;相应 地,模型中钨溶解度降幅可作为实际值的上限值。

模型所得出的 pH 范围处于弱酸性环境。在这种环境下, Wood 和 Sammon 得出的含钨组分以 HWO₄ 和 NaWO₄ 为主^[51]。这与模型计算结果 一致。

反应平衡模型计算结果表明,在4~8 km 的成 矿深度下,降压造成的 CO₂ 逃逸可使钨溶解度下 降 27%~47%;成矿流体温度越高,成矿深度越 大,钨溶解度降幅比例越大。位于葡萄牙的 Panasqueira 矿床是世界上最大的锡钨脉型矿床之 一,该矿床钨沉淀的效率只有 33%,剩余 67% 被 分散在矿体周边钨品位较低的围岩中^[56]。对比可 知,单纯的降压可显著降低钨在富含 CO₂ 热液中 的溶解度,因而是黑钨矿沉淀的有效机制。

致谢: 文章模型计算使用了毛世德教授提供的 CO₂ 溶解度计算程序和两个开源 R 语言程序包: Jeffrey Dick 开发的 CHNOSZ 和 Soetaert 开发的 rootSolve,在此一并表示感谢。

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